

Technical-Economic Justification Of The Efficiency Of Using The Heliopyrolisis Device In Heliothermic Processing Of Biomass

Almardanov Hamidulla Abdiganievich	Karshi Engineering Economics Institute, 180100, Karshi Uzbekistan						
Uzakov Gulom Norboevich	Karshi Engineering Economics Institute, 180100, Karshi Uzbekistan						
This article present concentrator heliopy for domestic needs of and farms) were a concentrator, an ave fuel and 200÷300 H consumers located f scientifically based.	is in order to evaluate the effectiveness of the parabolic solar prolysis device developed, the indicators of natural gas consumption fhouseholds and consumers located far from energy supply (farmers analyzed. Using a heliopyrolysis device with a parabolic solar rage of 300÷350 m ³ of gaseous fuel, 350÷400 kg of liquid pyrolysis kg of solid fuel per year for household needs of residents and far from the energy supply the availability of alternative fuels is						
Keywords:	Solar energy, parabolic concentrator, material balance, biomass						

pyrolysis, alternative fuel, solar pyrolysis plant.

Introduction

Natural gas consumption per capita in Uzbekistan is 3 times higher than in developed countries and neighboring countries. For comparison, in foreign countries, 90 m³ of gas per person per year is needed, while in Uzbekistan, this figure exceeds 400 m³. According to statistics, in 2018, 3,2 mln. more households than 10 billion m³ of gas were consumed in (14 mln. inhabitants). And this one the apartment year during heating and household needs for 5000 m³ gas is used means in the country of Belarus this indicator 1700-1900 m³ organize reaches [1-3].

Kashkadarya region opposite in the city built exemplary of houses heat and electricity supply system energetic analysis that's it shows that heating, hot water supply and electricity in supply traditional energy resources saving, stable respectively energy (heat and electricity energy) with to provide, especially heat in supply traditional (natural gas, coal, firewood and etc.) fuels share and ecological effect reduce such as problems. There is this in apartments household needs for expendable common gas spending per day maximum 4,5 m³ in case organize reaches [4-8].

Urban planning norms and according to the rules (ShNQ) (2.04.08-13 "Gas supply. Project norms") of gas accounting spending gas supply has been in the apartment gas plate when and centralized. Hot water supply and gaseous water space heater otherwise per 1 person per year $\bar{G}_{gas}^{y} = 6000 \frac{MJ}{year}$. Is as a result, 3 persons of the household household needs for 3x600 per year =18000 MJ/year, 614 kg conditional fuel or 490-500 m³ up to natural gas consumption does [9].

Exemplary houses and energy from supply away is located of consumers (farmer and farmer farms) household goods (food preparation, tea boiling, hot water and etc.) in natural gas supply traditional and again renewable, in particular the sun energy based

Volume 23 | October 2023

ISSN: 2795-7640

on working devices work exit and parameters justification important task is [10-14]. This task scientific based on without solve and it is considered an urgent task.

Method

In order to evaluate the effectiveness of the heliopyrolysis device with a parabolic solar concentrator developed in the article, the natural gas consumption indicators for domestic needs of households and consumers located far from the energy supply (farmers and farms) were analyzed (table 1). Table 1

Indicators of natural gas consumption for household needs in households										
Gas plate type	Parameters	Consumer type (144 m ² heating to the surface have waxy house)	Household needs for average gas consumption							
Artel Apetito 10-G	Oven volume: 65.0 l The work systems number: 2.0 Electric energy source: 220 V/50 Hz Stoves number: 4.0 Without packaging Dimensions (WxDxH): 850x600x600 Packaged Dimensions (WxDxH): 930x650x700 Without packaging weight :41.0 kg Packaged weight: 45.0 kg		I. Experimental results 7941,937 m ³ 09/14/2023 at 8:00 am 09/15/2023 at 8:00 am							
Artel Milagro 50 02-K Combined plate	Oven volume: 52.8 l Electric energy source: 220 V/50 Hz Upper TEN power: 1000.0 W Stoves number: 3.0 Electric comforters number: 1.0 Without packaging dimensions (ExChxB): 500x570x850 Packaged dimensions (ExChxB): 555x665x900 Without packaging weight: 31.7 kg		Daily real gas consumption:0,95 ÷ 1,1 m³/day.II.II."Hududgaztaminot"JSC statistician information:Opposite in the citysubscribers Number:65,000Household needs foraverage gas consumption:54,000 - 60,000 m³/dayDaily average gasconsumption: 0,83 - 0,92m³							

Volume 23 | October 2023

		Oven volume: 65.0 l	III. Sample (144 m ²
		The work systems	heating surface) of the
66646-		number: 2.0l	house natural gas costs
		Stoves Number: 4.0	(actual need):
		Without packaging	Daily : 0.95-1 m ³
	Artal Aratita	Dimensions (WxDxH):	Monthly : 28.5-30 m ³
		850x600x600	Year : 340-360 m ³
	00-G Gaz	Packaged Dimensions	
	plate	(WxDxH): 930x650x700	
		Without packaging	
		weight: 36.0 kg	
		Packaged weight: 40.0	
		kg	

The amount of gaseous fuels (pyrogas) released from biomass and organic waste V_{PG} , m³, is determined using the following expression:

$$\mathcal{W}_{PG} = n_s \cdot m_b \cdot g_{ek} \tag{1}$$

here, n_s –daily number of downloads, $n_s = 3$; m_b –product mass loaded into the reactor, kg; g_{ek} –The amount of pyrogas released from 1 kg of biomass or organic waste, $g_{eq} = 0,3\div0,45 \text{ m/kg}$ (experimental results).

The amount of pyrogas released from biomass and organic waste per month is determined as follows in the sunny months of the year:

$$V_{PG}^{mon} = 30 \cdot V_{PG} \tag{2}$$

The reactor of the heliopyrolysis device is cylindrical, and its dimensions are mainly determined by the ratio of its height to its internal diameter (h/d = 0.9...1.3). If we assume that h/d = 1, then the following equation is formed:

$$V_r = \frac{\pi d_r^2}{4} \cdot h = \frac{\pi d_r^2}{4} \cdot d_r$$
$$d = \sqrt[3]{\frac{4V_b}{\pi}} = \sqrt[3]{\frac{4\cdot 1,3}{3,14}} = 0,2 m$$
(3)

The amount of heat used to heat the biomass or organic waste to the pyrolysis process Q_{heat} , MJ, is determined as follows:

$$Q_{heat} = c_b \cdot m_b \cdot (t_{pyr} - t_{ext}) \tag{4}$$

here, c_b –heat capacity of biomass or organic waste , $\frac{J}{kg \cdot \circ C}$; t_{pyr} –temperature of the pyrolysis process (350÷500 °C); t_{ext} –external temperature, °C.

The average monthly amount of heat used to heat biomass or organic waste is determined as follows:

$$Q_{heat}^{mon} = Q_{heat} \cdot \tau_{day.mon} \tag{5}$$

Here, $\tau_{day.mon}$ –monthly number of sunny days.

Side walls of the reactor to be lost heat quantity Q_{lost} , MJ, q in the house from the formula defined as:

$$Q_{lost} = k \cdot F_{reak} \cdot (t_{pyr}(\tau) - t_{ext})$$
(6)

this on the ground , k –the heat transfer coefficient, $\frac{Vt}{m^{2} \cdot c}$; F_{reak} –the surface of the side of the reactor, m^2 ; monthly t_{ext} –average of the external environment temperature, °C; $d\tau$ – pyrolysis process time, sec.

Heliopyrolysis device reactor for heat transmission coefficient the following equation using is:

$$k = \frac{1}{\frac{1}{\alpha_n} + \frac{\delta_r}{\lambda_r} + \frac{1}{\alpha_k}}, \frac{Vt}{m^{2.\circ}C}$$
(7)

this on the ground α_n –light heat transfer to give coefficient $\frac{Vt}{m^{2.0}C}$; α_k - convective heat transfer to give coefficient $\frac{Vt}{m^{2} \cdot C}$; of δ_r –reactor material thickness, m; λ_r –reactor material heat permeability coefficient, $\frac{\sqrt{n}}{m \cdot \circ C}$.

Monthly amount of heat lost from Q_{lost}^{mon} the reactor , MJ, determined from the following formula: $Q_{lost}^{mon} = Q_{lost} \cdot \tau_{day.mon}$ (8)Pyrolysis process for demand to be done common energy quantity as follows defined as:

0

$$Q_{dem} = Q_{heat}^{mon} + Q_{lost}^{mon}, MJ/month$$
(9)

. .

Results and discussion

- - **-**

Above from expressions used without calculated the results are presented in table 2.

Table 2.

r	Months in the section work issued gaseous amount of fuel (pyrogas).											
Month	1	2	3	4	5	6	7	8	9	10	11	12
S												
t _{ext} , ℃	6.3	9.2	16.4	22.6	28.7	33.1	38.9	36.8	30.5	20.6	13.3	8.1
$\tau_{day.mon}$	10	9	11	13	22	30	31	31	30	27	15	15
Q _{heat} , MJ/ month	71.6	64.4	78.7	93.0	157. 4	214. 7	221. 8	221. 8	214. 7	193. 2	107. 3	107.3
Q _{lost} , MJ/ month	25.0	22.5	27.5	32.5	54.9	74.9	77.4	77.4	74.9	67.4	37.5	37.5
Q ^x _{sp.y,} MJ/mon	96.5	86.9	106. 2	125. 5	212. 4	289. 6	299. 2	299. 2	289. 6	260. 6	144. 8	144.8
V ^{mon} , m ³ /mont	13.5	12,1 5	14.8 5	17.5 5	29.7	40.5	41,8 5_	41.8 5	40.5	36.4 5	20.2 5	20.2 5

Experience to the results according to parabolic the sun concentrator heliopyrolysis on the device months in the section work issued liquid and char (active coal) fuel amounts are in tables 3 and 4. Table 3.

Months in the section work issued liquid biofuel quantity												
Months	1	2	3	4	5	6	7	8	9	10	11	12
Rubber	6.6	5.4	6.6	8.4	13.8	18	18.6	18.6	18	16.8	9	9
waste, kg												
Poultry	3.3	2.7	3.3	4.2	6.9	9	9.3	9.3	9	8.4	4.5	4.5
manure, kg												
Polyethyle	18.5	14.85	18.5	23.1	37.95	49.5	51.1	51.1	49.	46.2	24.7	24.7
ne film, kg							5	5	5			
Plastic	10.8	8.9	10.8	13.8	22.7	29.7	30.6	30.6	29.	27.7	14.8	14.8
bottle, kg									7			
Plant waste	8.5	7.02	8.5	10.9	17.9	23.4	24.1	24.1	23.	21.8	11.7	11.7
(cotton									4			
stalk), kg												

Table 4

Months in the section work issued char fuel quantity												
Months	1	2	3	4	5	6	7	8	9	10	11	12
Rubber	14.8	12.1	14.8	18.9	31.1	40.5	41.8	40.5	40.5	37.8	20.2	20.2
waste, kg												
Poultry	11.2	9.1	11.2	14.2	23.4	30.6	31.6	31.6	30.6	28.6	15.3	15.3
manure, kg												
Coal	13.2	10.8	13.2	16.8	27.6	36	36	37.2	36	33.6	18	18
Plastic	8.9	7.2	8.9	11.3	18.6	24.3	25.1	25.1	24.3	22.8	12.1	12.1
bottle, kg												
Plant	12.2	10.2	12.3	15.6	24.1	31.6	32.6	32.6	31.6	29.3	16.1	16.4
waste												
(cotton												
stalk) , kg												

Conclusion

So is done research and count results that's it shows that the offer done the sun concentrator heliopyrolysis device using one up to 3 kg per day raw material again worked. Kashkadarya in the region in the area yearly sunny 300 days that acceptance if we do, one in minimum 300x3=900 kg raw the item again work can. So, this one device using one 900÷1000 kg of biomass per year or organic waste heliothermic again work opportunity is created. As a result parabolic the solar concentrator heliopyrolysis device using per year for household needs of consumers located in households and far from energy supply on average 300÷350 m³ gaseous fuel, 350÷400 kg liquid pyrolysis fuel heat and 200÷300 kg up to char alternative fuel get possible was determined.

References

- Uzakov G.N., Novik A.V., Davlonov X.A., Almardanov X.A., Chuliev S.E. Heat and Material Balance of Heliopyrolysis Device. ENERGETIKA. Proceedings of CIS higher education institutions and power engineering associations. 2023; 66(1):57-65. <u>https://doi.org/10.21122/1029-7448-</u> 2023-66-1-57-65
- 2. Uzakov, G.N., Almardanov, X.A., Kodirov, I.N., Aliyarova, L.A. Studying the temperature regime of the heliopyrolysis device reactor. E3S Web of Conferences,

2023, 411, 01040 DOI: 10.1051/e3sconf/202341101040

- 3. Xayrulla Davlonov, Xamidulla Almardanov, Inomjon Khatamov, Sadriddin Urunboev, Palvan Kalandarov, and Orif Olimov, "Study on heat and material balance of heliopyrolysis device", AIP Conference Proceedings 2686, 020023 (2022) https://doi.org/10.1063/5.0111855
- Almardanov, X. A., et al. "Application of solar concentrators to obtain alternative fuel through a heliopyrolysis device." Universum: Technical Sciences 3 (2021): 8-12.
- 5. Almardanov, H. and Chuliyev, S. 2022. Biomassadan geliopiroliz usulida yoqilgʻi olish tajriba qurilmasining parametrlarini asoslash. Innovatsion texnologiyalar. 1, 4 (Nov. 2022), 92–96.
- 6. Davlonov, X. A., X. A. Almardanov, and I. A. Khatamov. "A program for modeling and calculating the exergic balance of a heliopyrolysis device to obtain alternative fuels from biomass." No DGU 10337 (2021).
- Sh.B. Imomov, X.A. Alimardonov. Heat mode solar heating systems based on flat reflectors, sets on the north side of the building. Молодой ученый, 2015, 335-336 ст.
- 8. Davlonov X.A., Almardanov H.A., Toshboyev A.R., Umirov F.B. Method of Thermal Processing of Biomass With Heliopyrolysis Device. 2021,

International Journal of Human Computing Studies, 3(2), 149-151.

- 9. ShNQ 2.04.08-13 «Gaz ta'minoti. Loyiha normalari.» Tashkent shahri, 2013. Davarxitektqurilish OʻzR.
- 10. Алмарданов Хамидулла Абдиғаниевич, Хатамов Иномжон Амруллаевич, Тураев Зухриддин Баходирович, Эшонкулов Мансур Насим Угли, Жовлиев Сарвар Мустафо Угли. and Юсупов Рустам Эшпулатович. "ПРИМЕНЕНИЕ СОЛНЕЧНЫХ КОНЦЕНТРАТОРОВ ДЛЯ АЛЬТЕРНАТИВНОГО ПРИЕМА **УСТРОЙСТВО** ТОПЛИВА ЧЕРЕЗ ГЕЛИОПИРОЛИЗА" Universum: технические науки, по. 3-4 (84), 2021, pp. 8-11.
- 11. Давлонов X.A., Алмарданов X.A., Гадоев C.A., Шаймарданов И.З. Исследование теплового режима процесса гелиопиролиза биомасса // Универсум: технические науки: электрон. научн. журн. 2021. 4(85) 5-8 СТ.

https://7universum.com/ru/tech/archi ve/item/11550

- 12. Узаков Г.Н., Новик А.В., Давлонов Х.А., Алмарданов Х.А., Чулиев С.Э. Тепловой и материальный баланс гелиопиролизного устройства. Энергетика. Известия высших учебных заведений и энергетических объединений СНГ. 2023;66(1):57-65. <u>https://doi.org/10.21122/1029-7448-2023-66-1-57-65</u>
- 13. Т.Я. Хамраев, Х.А. Алмарданов. Режим работы установок для получения биогаза из селскохозяйственных отходов. Молодой ученый. — 2020. — № 25 (315). — С. 49-52.
- 14. К.К. Рахимова, Х.А. Алмарданов, С.И. Хамраев, С.М. Шамуратова, А.Р. Тошбоев, Э.Э. Турдиев. Теплоснабжение и энергосбережение сельскохозяйственных сооружений с пассивной системой солнечного отопления. ГГТУ им. ПО Сухого, 2020, 242-245 ст.